

UNITED STATES PATENT APPLICATION

OF

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FOR

**METHOD FOR MAXIMIZING WATER REMOVAL IN A PRESS NIP**

## METHOD FOR MAXIMIZING WATER REMOVAL IN A PRESS NIP

### RELATED CASES

This application is a continuation-in-part of copending application Serial No. 09/191,376, filed November 13, 1998.

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### FIELD OF INVENTION

The invention relates to a method for maximizing water removal from an absorbent paper web in a press nip. More particularly, the present invention relates to the use of a shoe press on the Yankee dryer with a pressure profile that maximizes water removal. Still more particularly, the present invention relates to a method for utilizing a very steep pressure drop at and/or following the exit of a nip curve in order to maximize water removal by minimizing rewet. Finally, the present invention relates to a method for increasing paper machine speed by utilizing a press section that maximizes water removal.

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### BACKGROUND OF THE INVENTION

In modern society, bath tissue, paper towels, facial tissue, and paper napkins (hereinafter referred to as packaged paper products) have been remarkably successfully consumer products. The success of these paper products stems from the ability of manufacturers to consistently enhance product attributes at lower cost and to meet volume demands on a timely basis. Packaged paper products offer consumers

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5 an array of attributes necessary to such jobs as performing the daily tasks of wiping up  
spills, personal cleansing, and cleaning household goods. For example, paper towels  
are engineered to be absorbent and strong while wet whereas bath tissue products are  
expected to be soft to the touch yet strong while in use. Absorbency and softness are  
inversely related to strength, often making it difficult to obtain the right balance of  
10 attributes. Accordingly, significant research and development efforts are routinely  
expended to enhance the quality of these products while continuing to reduce cost by,  
for example, improving the production of these products. Although numerous schemes  
have been developed and patented, the search by R&D departments continues to seek  
out new and innovative methods for improving these products.

15 There are numerous methods described in the patent literature for improving the  
quality of packaged paper products. One of the earliest known methods to enhance the  
quality of consumer paper products is described in U. S. Patent No. 3,301,746 by  
Sanford and Sisson, assigned to Procter and Gamble Corporation, and incorporated  
herein by reference in its entirety. This patent describes a papermaking scheme for  
20 enhancing product quality by avoiding overall web compression and by using a pattern  
array of densified regions in the xy plane of the sheet to enhance product strength.

25 Other early methods for improving the quality of packaged paper products are  
described in U.S. Patent No. 3,812,000 by Salvucci and Yiannos and U.S. Patent No.  
3,821,068 by Shaw. These patents are assigned to Scott Paper Company, each of  
which is incorporated herein by reference in its entirety. Shaw discloses a papermaking  
scheme for producing soft tissue by avoiding mechanical compression until the sheet

5 has been dried to at least 80% solids. Salvucci and Yiannos disclose a technique for producing a soft tissue structure by avoiding mechanical compression of an elastomeric containing fiber furnish until the consistency of the web is at least 80% solids.

10 Thicker more absorbent structures can be made using a low batting papermaking felt as described in U.S. Patent No. 4,533,457 by Curran et al., assigned to Scott Paper Company, and incorporated herein by reference in its entirety. U.S. Patent Nos. 5,591,305 and 5,569,358 by Cameron, assigned to James River Corporation, and incorporated herein by reference in their entirety, disclose a low-batting, high-bulk-generating felt with improved dewatering capabilities.

15 A more recent method for improving the quality of a through-air-dried sheet is described in U.S. Patent No. 4,440,597 by Wells and Hensler, assigned to Procter and Gamble Company, and incorporated herein by reference in its entirety. This patent describes a method for increasing the stretch of a paper web by operating the forming section of a paper machine faster than the through air dryer section of the paper machine. As a result of the speed differential, the paper web is inundated into the through air-dryer-fabric leading to enhanced stretch and absorbency properties in the 20 base sheet and resulting product.

25 Fibers and chemicals can be used to enhance the quality of packaged paper products. For example, U.S. Patent No. 5,320,710 by Reeves et al., assigned to Fort James Corporation, and incorporated herein by reference in its entirety, describes a new furnish combination extracted from the species *Funifera* of the genus *Hesporaloe* in the Agavaceae family. This furnish has fibers which are very long and which have

5 very fine-geometrical attributes known to enhance tissue and towel performance. U.S. Patent No. 3,755,220 by Freimark and Schafflein, assigned to Scott Paper Company, and incorporated herein by reference in its entirety, describes a debonding scheme for maintaining wet strength while reducing product dry strength-a method known to enhance the handfeel of towel products.

10 The use of bulking fibers can improve the quality of the final end product. U.S. Patent No. 3,434,918 by Bernardin, U.S. Patent No. 4,204,504 by Lesas et al., U.S. Patent No. 4,431,481 by Drach et al., U.S. Patent No. 3,819,470 by Shaw et al., and U.S. Patent No. 5,087,324 by Awofeso et al. disclose the use of bulking fibers in papermaking webs to improve product attributes like thickness, absorbency, and softness. These aforementioned patents are incorporated herein by reference in their entirety.

15 U.S. Patent No. 5,348,620 by Hermans et al., assigned to Kimberly-Clark Worldwide Inc., and incorporated herein by reference discusses a high consistency/high temperature fiber-treatment-process using a disperser to improve product attributes. To improve tissue softness, several approaches are available to the papermaker such as using certain species of hardwood like eucalyptus in stratified webs as disclosed in U.S. Patent No. 4,300,981 by Carstens and U.S. Patent No. 3,994,771 by Morgan et al. The last two patents are incorporated herein by reference in their entirety. These aforementioned patents describe just a few of the many methods developed over the last thirty years to enhance the quality of packaged paper products.

20 25 There are also numerous schemes for enhancing the productivity of paper

5 machines. For example, gap formers have been developed to enhance sheet drainage ultimately leading to increased machine speed. New developments in Yankee hood design and Yankee cylinder design have allowed improvements in heat transfer coefficients and mass transfer coefficients, ultimately leading to enhanced machine speeds. New developments in forming fabrics, e.g., multi-layer and triple-layer forming fabrics, have resulted in improved drainage, better fabric life, and enhanced fiber support. These factors translate into enhanced machine speed and productivity. Improvements in press felts, e.g. Scapa's SPECTRA™ felt concept of using a soft polyurethane sandwich near the base of the felt or the use of stratified batting, have led to improvements in felt life, reductions in break-in time, and improvements in water removal at wet presses. These improved press-felt developments have ultimately translated into improved machine speed and productivity. Improvements in Yankee creping adhesives have been helpful to enhance blade wear and reduce sheet plugging. Continuous creping doctors have alleviated the need to frequently change doctor blades. The last two aforementioned developments have led to improvements in machine speed, reductions in down time, and reductions in paper waste. In spite of all these advances, methods are sought to enhance productivity.

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25 The present invention improves the efficiency of known water removal methods by adding one or more pressing units to the production paper machine, in place of or in conjunction with a suction pressure roll. "Pressing units" according to the present invention include those units that physically engage a belt or pressing blanket, which contacts the impression fabric or felt upon which the web travels. "Foraminous endless

5 fabric" as defined in accordance with the present invention includes either an  
impression fabric or felt. "Pressing unit" as defined in accordance with the present  
invention includes any press members allowing deformation of the pressing  
blanket/impresion fabric and/or felt/web sandwich to result in asymmetric pressure  
profiles. These pressing units including pressing blankets are generally discussed in the  
10 literature as "shoe presses." Pressing units according to the present invention do not  
include suction pressure rolls since they lead to symmetrical pressure distributions  
frequently mathematically described by sine or haversine functions.

15 Shoe presses have been used to increase water removal at wet presses,  
ultimately leading to increased machine speed for linerboard grades and more recently,  
newsprint and fine paper grades. The idea of extending the time in a press nip as a  
means to enhance water removal is not a new idea. Nissan in 1954 published a paper  
in Tappi, Vol. 37, No.12, p.597 (1954) suggesting that the use of extended time in a  
press nip would enhance the water removal performance of a press. Over twenty-five  
years, ago Busker published an early paper in Tappi, Vol. 54, No.3, p.373 (1971) on the  
20 use of extended nip times, as a means to enhance water removal. Beloit Corporation  
commercialized the first open belt wide shoe press on a linerboard machine in 1980 as  
described in an article by J. Blackledge presented during the 2<sup>nd</sup> International Pira  
Conference, entitled 'Modern Technologies in Pressing and Drying', Nov 6-8, 1990, p.

25 1. The aforementioned three articles are herein incorporated by reference in their  
entirety.

Figure 1 shows a typical closed belt wide shoe press (see Figure 2 in an article

entitled "New Pressing Technologies for Multiply Board" by J. Breiten in 81<sup>st</sup> Annual Meeting, Technical Section, CPPA, p. A137 for a more detailed drawing). A wide shoe press as described in the literature is essentially a controlled crown roll with a flexible shell and a concave shoe hydrodynamically loaded against each other. The belt or blanket is usually a fabric reinforced polyurethane-coated structure that can be grooved or blind drilled for more efficient water removal. The inside of the belt is generally lubricated with oil, which develops a hydrodynamic film as it passes over the shoe and reduces wear/friction in both surfaces. Wide shoe press nips are on average 5 to 10 times longer than conventional roll press nips (generally, 5" – 10" versus 1" – 2"). Water deflectors (not shown) on the outside surface will dewater the blanket. By utilizing such a wide nip, loads up to 10,000 pli are possible without the risk of damaging blankets and felts or crushing the sheet. The exit side of the shoe features a sharply curved nose designed to pull the sheet directly out of the nip and away from the felt, thus reducing rewet and improving sheet dryness. U.S. Patent No. 4,931,142 describes certain advantages to this type of take off angle in conjunction with long press nips. Rolls do not normally support the belt loop of the wide shoe press. The loop generally is closed off with special head assemblies for containing the oil.

Numerous schemes for improving the operation of shoe presses have been developed over the years. For example, in U.S. Patent No. 5,043,046 by Laapotti and assigned to Valmet Corporation, U.S. Patent No. 4,625,376 by Schiel et al. and assigned to Voith Corporation, and U.S. Patent No. 4,673,461 by Roerig and assigned to Beloit Corporation, methods are described to enclose the shoe press in order to

5 contain the oil within the unit. The previous three patents are incorporated herein by reference. U.S. Patent No. 5,167,768 by Cronin and Roerig and assigned to Beloit Corporation and U.S. Patent No. 5,582,689 by Rolf Van Haag and Hans-Rolf Conard and assigned to Voith Corporation describe methods for varying the pressure distribution in a shoe press. This capability avoids the need to offset the center of  
10 loading or reshape the shoe to change the pressure distribution. These last two patents are also incorporated herein by reference. U.S. Patent No. 5,693,186 by Vallius, assigned to Valmet Corporation, and incorporated herein by reference describes a tension link scheme for containing the loading within the framing of the  
15 shoe press apparatus. This scheme ultimately avoids the need to fortify flooring when operating at high line loads. These are just a few of the many developments that have led to improved operating shoe presses.

20 In the art of pressing linerboard, newsprint, and fine paper webs with a shoe press, a long shoe with a gradual pressure rise is desirable for good dewatering and enhanced bulk properties. This is especially true for flow controlled webs. Linerboard and to a certain extent newsprint and fine paper have flow controlled pressing conditions. Flow controlled pressing conditions occur when the time in the nip becomes an important factor determining the amount of water removed from the web. High pressure can be attained with these long shoes but it requires high line loads. Figure 2 shows the relationship between peak pressure (i.e., the maximum pressure in the nip) and line load (i.e., the total force divided by linear width) for shoe press nips compiled  
25 from an extensive but not exhaustive search of the literature. Table I describes the

literature references used to develop Figure 2.

Table I: References Used to Generate Figure 2.

Reference Number	Source
1	U.S. Patent No. 5,167,768
2	W. Schuwerk, Paper Age, September, 1997, p.18.
3	N. Anderson, Journal of Tappi, Vol. 21, No. 1, 1998, p.52.
4	J. Kinnunen and A. Kiviranta, Paperi Ja Puu-Paper and Timber Vol. 74, No. 4, 1992, p. 314.
5	J. Kivimaa, M. Laurikainen, and K. Pansu, PITA Water Removal Conference 1997 York, Paper Technology, April, 1998.
6	J. Blacklege and D. Lange, 2 <sup>nd</sup> International Pira Conference, "Modern Technologies in Pressing and Drying", Nov. 6-8, 1990, p.1.
7	M. Radtke, 79 <sup>th</sup> Annual Meeting, Technical Section, CPPA, p. A221.
8	J. Breiten, 81 <sup>st</sup> Annual Meeting, Technical Section, CPPA, p. A137.
9	E. Tenfalt , J. Wilmenius, and O. Swanberg, Nordic Pulp and Paper Research Journal, 1998, p.16.
10	D. Lange and M. Radtke, Papermaker, July 1996, p. 16.
11	"Chemical Systems Boost Dry Content", PPI, February, 1989, p. 41.

The graph in Figure 2 shows that shoe presses normally operate at high line load conditions, usually greater than 270kN/m and at high peak pressures. It also shows that shoe presses are not operated at low line loads and at high peak pressures (e.g., see the crosshatched region in Figure 2).

In the art of making tissue by the conventional wet pressing operation, Yankee dryers are loaded with suction pressure rolls to remove water from the tissue web and attach the web to the dryer for further processing by the creping operation. The

5 pressure distribution in the suction pressure roll nip is symmetrical in shape and is  
described mathematically by a sine or a haversine curve. Suction pressure rolls loaded  
to a Yankee dryer are routinely run at line loads less than 100 kN/m and at peak  
pressures of less than 4500 kN/m<sup>2</sup>. In the lower left-hand corner of Figure 2 some  
typical peak pressure versus line load data for suction pressure rolls are shown. The  
10 deflection of large, conventional Yankee dryers due to hoop stress levels limits the line  
load to less than about 100 kN/m. As a result, it is very difficult to attain high peak  
pressures in the nip at these low line loads, since the pressure distribution cannot be  
altered. This limitation has extreme consequences for tissue grades since they are  
15 pressure controlled, i.e., the flow resistance in the web is low due to the use of high  
freeness furnishes and low basis weight webs, thus it is believed that peak pressure,  
not time in the nip, controls press dewatering. These suction pressure rolls suffer from  
other disadvantages. For example, since the nip diverges after the maximum pressure  
is achieved, rewet can occur for a large part of the press nip. A typical suction pressure  
roll curve appears in Figure 3, where nip divergence is apparent. Also, the suction  
20 pressure roll unit is not flexible so that the line load needs to be fixed and matched to a  
given Yankee crown condition in order to obtain a uniform nip profile across the  
machine. Furthermore, since the loading cylinders are located at each end of the  
pressure roll, profiling capabilities are very limited.

25 The use of conventional shoe presses on a Yankee dryer at the maximum hoop  
stress limit of 100kN/m would lead to very low peak pressures as Figures 2 and 3  
demonstrate. For example, with a 120 mm shoe at 100 kN/m, the typical peak pressure

5 is on the order of 1700 kN/m as Figure 3 demonstrates. Since the press nip for low weight tissue and towel grades is pressure controlled, the very low peak pressure could cause a decrease in post press dryness, ultimately causing a loss in production. The counter roll in a conventional shoe press is small by comparison to the diameter of a Yankee dryer. As a result, the use of a conventional shoe shape would make it very  
10 difficult to remove the felt/fabric from the sheet at the nip exit. Therefore, conventional shoe shapes and conventional felt/fabric takeoff angles would exacerbate rewet for low weight absorbent products.

15 Currently, there are no commercial uses of shoe press technology in the production of absorbent paper products. U.S. Patent No. 5,795,440 by Ampulski et al., and U.S. Patent No. 5,776,307 by Ampulski et al.-both assigned to Procter and Gamble Corporation and both incorporated herein by reference, describe a scheme for making a shaped web by pressing an embryonic web into an imprinting fabric between two felts. These patents use a shoe press assembly in the preparation of a wet pressed paper web. Ampulski et al., like others using pressing units, teaches the use of longer conventional press nips. Ampulski et al. discloses that the nip length is greater than 3.0  
20 inches and may be as long as 20.0 inches. Ampulski et al. achieves this extended nip length through the use of a shoe press. Ampulski et al., like all previous users of shoe presses, fails to consider the use of increased peak pressure.

International patent application WO 97/43483 by Hermans and Friedbaurer,

assigned to Kimberly-Clark Worldwide, Inc., and incorporated herein by reference discloses that extended nip presses, while having been successfully used for making paperboard, have not been used to make low density paper products such as tissue because the high pressure and longer dwell times in an extended nip press serve to densify the sheet beyond that experienced by conventional tissue wet pressing methods. Hermans and Friedbaurer overcome the increased density due to extended nip pressing by incorporating modified resilient fibers (e.g., chemically cross-linked cellulosic fibers) in the web and by wet micro-shaping the web. They also disclose shoe lengths typically in the range of 5 to 10 inches. Like Ampulski et al., Hermans and Friedbaurer do not consider critical peak pressures or line loads as important.

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U.S. Patent No. 5,393,384 by Steiner et al., and assigned to J.M. Voith, GmbH (hereinafter "the '384 patent") generally describes the use of a shoe press in the production of a tissue web. The '384 patent describes the use of a shoe press preceding or contacting a Yankee drying cylinder. The shoe press is used in conjunction with an impermeable belt to reduce remoistening of the sheet by the felt. These authors used the impermeable belt since they state: "the prevailing opinion in selecting suitable drying presses in contingence on the web thickness so far has been that for drying thin webs there are only simple roll presses suited which generate a sufficiently high contact pressure for a short time, thus optimally removing the water from a thin web (tissue web) due to the short path, whereas shoe type presses are suited essentially for drying thick, heavy webs, since they generate a persistent

5 pressure which allows the water sufficient time for the considerable longer path in leaving the web." Critical peak pressure and line loads are not discussed in the disclosure. Since the shoe press described in this disclosure is conventional, a pressure curve for this type of shoe press is most likely similar to the "typical shoe press curve" illustrated in Figure 3.

10 Voith, the assignee of the '384 patent, continues to develop the use of a shoe press for the production of paper products. U.S. Patent No. 5,500,092 by Schiel describes a tissue making machine using a triple press nip where the second nip is a shoe press nip. The criticality of pressure distribution shape and peak pressure/line load magnitudes are not disclosed in the '092 patent. In the September 1997 article W. 15 Schuwerk, "Shoe Presses and Sleeves for Newsprint-Concepts and Initial Operating Experience," PaperAge, Pp. 18-23, Voith described the advantages of their NIPCOFLEX shoe press. According to that article, "[T]o obtain optimum product characteristics, dewatering in the press must [therefore] show as flat a pressure gradient as possible." In fact, the shoe press described in the article refers to the third section of a newsprint paper machine operating at a line loading of 850 kN/m and a 20 peak pressure of ~5.6 MPa, typical of standard conventional shoe designs and well outside the range of the present invention.

25 U.S. Patent No. 4,931,142 by Steiner, Muller, Schiel, and Flamig, assigned to Voith Corporation and incorporated herein by reference in its entirety describes a method of eccentrically arranging a press blanket with respect to the press plane. This arrangement enables the blanket upon leaving the press nip to immediately move

5 steeply downward and away from the sheet in order to reduce remoistening of the web.  
Methods of varying the felt angle with respect to the traveling web in a double felted  
press nip were disclosed to avoid remoistening the sheet and for quick release of the  
sheet from the felt. Steiner et al. also discloses that the joint path of travel of the paper  
web, felt, and blanket can be made substantially shorter than prior art. By utilizing the  
10 Steiner et al. invention, the joint travel of the felt, web, and blanket can be made equal  
to zero, i.e., the web can detach itself from the felt directly at the emergence from the  
press nip. Steiner et al. does not address low line loads and high peak pressures  
needed for optimum shoe press performance on Yankee dryers. It also does not  
disclose the need to taper the press shoe to achieve minimized rewet.

15 U.S. Patent No. 5,556,511 by Bluhm and Gotz, assigned to Sulzer-Escher Wyss,  
and incorporated herein by reference describes a process for making toilet tissue webs  
whereby a web is wet pressed in a heated pressing arrangement. The heated pressing  
arrangement can be a shoe press. This disclosure does not address the importance of  
proper choice of peak pressure, line load, and shoe shape for making absorbent  
20 products at high speeds. In fact, the critically of line loads and peak pressures is not  
discussed. Bluhm and Gotz like all previous users of shoe presses, fails to consider the  
use of increased peak pressure at low line loads as a means to improve water removal.

25 U.S. Patent No. 4,973,384 by Crouse, Pulkowski, and Porter, assigned to Beloit  
Corporation, and incorporated herein by reference describes a process for using a  
heated extended nip press for optimizing sheet properties without lamination. To  
accomplish the aforementioned task Crouse et al. found that by application of pressure

5 for an increased period of time, the increased residence time enables the removal of  
more water from the formed web. As a result, these authors teach toward the use of a  
conventional long shoe design. They also found that for a heated extended nip press  
by "gradually decreasing pressure in machine direction toward the trailing edge of the  
shoe, rapid flashing of steam from the emerging pressed web was avoided." As a  
10 result these authors teach away from the use of a heavy peaked pressure distribution at  
the exit side of a shoe press nip.

WO 97/16593 by Wedel and Worcester incorporated herein by reference  
discloses an impulse drying method for tissue structures using a shoe press and an  
induction heater. This disclosed impulse-drying method is intended to replace the  
15 Yankee dryer with its associated problems. These authors list the issues with Yankee  
dryers as being limited in surface temperature to 185°F, as being limited in line load to  
500 pli due to shell thickness limitations, and as being limited in roll diameter. These  
authors state that shoe length is typically ten inches for the impulse drying unit. The  
line loads disclosed are 1000 pli to 10,000 pli. As a result, this application teaches away  
20 from the combined use of a low line load with a substantial peak pressure.

Contrary to the current state of the art, the present inventors have, quite  
unexpectedly, found that in the production of absorbent paper products, the use of a  
steep, sharp pressure gradient and controlled separation when producing absorbent  
paper can improve dewatering efficiency without adversely affecting product properties.  
25 An example of the pressure profile of the new shoe design for absorbent paper  
production according to the present invention is illustrated in Figure 3.

5 The present inventors unexpectedly discovered that good sheet dewatering and appropriate bulk/strength properties for low weight absorbent products could be attained with this pressure optimized shoe press. The optimized pressure conditions can be achieved according to the present invention by shaping the shoe, tilting the shoe in the shoe press, reducing the length of the shoe in the shoe press, and/or tapering the 10 exit side of the shoe. In addition, these conditions can also be achieved by deflecting the pressing blanket from the web carrying foraminous-endless-fabric at a point nearly simultaneous with separation of the foraminous-endless-fabric from the nascent web, thereby reducing rewet. These techniques enable the pressure optimized shoe press according to the present invention to achieve improved dewatering while maintaining 15 bulk with line loads less than about 240kN/m and peak pressures greater than about 2000 kN/m<sup>2</sup>.

## SUMMARY OF THE INVENTION

Further advantages of the invention will be set forth in part in the description, which follows and in part will be apparent from the description. The advantages of the invention may be realized and attained by means of the instrumentalities and combinations particularly pointed out in the appended claims.

To achieve the foregoing advantages and in accordance with the purpose of the invention, as embodied and broadly described herein, there is disclosed:

25 An apparatus for forming an absorbent paper sheet product comprising:  
a moving foraminous endless fabric;

5 means for depositing a nascent web for the absorbent paper sheet on the  
foraminous endless fabric;  
a moving endless pressing blanket;  
a Yankee drying cylinder; and  
a pressing unit engaging the pressing blanket adapted to urge the nascent web  
10 for the absorbent paper sheet on the foraminous endless fabric into engagement with  
the Yankee drying cylinder thereby forming a nip, the pressing unit being configured to  
create a peak engagement pressure of at least about 2000 kN/m<sup>2</sup> at an overall line load  
of less than about 240 kN/m.

15 There is further disclosed:

An apparatus for forming an absorbent paper sheet product comprising:  
a moving foraminous endless fabric;  
means for depositing a nascent web for the absorbent paper sheet on the  
foraminous endless fabric;  
a moving endless pressing blanket;  
a Yankee drying cylinder; and  
20 a pressing unit engaging the pressing blanket adapted to urge the nascent web  
for the absorbent paper sheet on the foraminous endless fabric into engagement with  
the Yankee drying cylinder thereby forming a nip, the pressing unit being configured to  
create a peak engagement pressure of at least about 2000 kN/m<sup>2</sup> at an overall line load  
of less than about 240 kN/m,

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the pressing unit being configured to disengage the web from the foraminous endless fabric such that rewet of the nascent web by the foraminous endless fabric is less than about 50% of the rewet predicted by the Sweet equations based upon the properties of the foraminous endless fabric and the nascent web.

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There is still further disclosed:

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An apparatus for forming an absorbent paper sheet product comprising:

a moving foraminous endless fabric;

means for depositing a nascent web for the absorbent paper sheet on the foraminous endless fabric;

a moving endless pressing blanket;

a Yankee drying cylinder; and

a pressing unit engaging the pressing blanket adapted to urge the nascent web for the absorbent paper sheet on the foraminous endless fabric into engagement with the Yankee drying cylinder thereby forming a nip, the pressing unit being configured to create a peak engagement pressure of at least about 2000 kN/m<sup>2</sup> at an overall line load of less than about 240 kN/m,

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the pressing unit being configured to both disengage the web from the foraminous endless fabric and disengage the foraminous endless fabric from the pressing blanket at a nip length of less than about one inch from the point the nip pressure reaches zero.

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There is still further disclosed:

An apparatus for forming an absorbent paper sheet product comprising:

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a moving foraminous endless fabric;

means for depositing a nascent web for the absorbent paper sheet on the foraminous endless fabric;

a moving endless pressing blanket;

a transfer cylinder; and

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a pressing unit engaging the pressing blanket adapted to urge the nascent web for the absorbent paper sheet on the foraminous endless fabric into engagement with the transfer cylinder thereby forming a nip, the pressing unit being configured to create a peak engagement pressure of at least about 2000 kN/m<sup>2</sup> at an overall line load of less than about 240 kN/m.

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There is still further disclosed:

An apparatus for forming an absorbent paper sheet product comprising:

a moving foraminous endless fabric;

means for depositing a nascent web for the absorbent paper sheet on the foraminous endless fabric;

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a moving endless pressing blanket;

a transfer cylinder; and

a pressing unit engaging the pressing blanket adapted to urge the nascent web for the absorbent paper sheet on the foraminous endless fabric into engagement with the transfer cylinder thereby forming a nip, the pressing unit being configured to create a peak engagement pressure of at least about 2000 kN/m<sup>2</sup>.

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There is still further disclosed:

5 An apparatus for forming an absorbent paper sheet product comprising:  
a moving foraminous endless fabric;  
means for depositing a nascent web for the absorbent paper sheet on the  
foraminous endless fabric;  
a moving endless pressing blanket;  
10 a backing roll; and  
a pressing unit engaging the pressing blanket adapted to urge the nascent web  
for the absorbent paper sheet on the foraminous endless fabric into engagement with  
the backing roll thereby forming a nip, the pressing unit being configured to create a  
peak engagement pressure of at least about 2000 kN/m<sup>2</sup> at an overall line load of less  
than about 240 kN/m.

15 There is still further disclosed:  
A method of making an absorbent paper sheet product comprising:  
depositing a nascent web for the absorbent paper sheet product on a moving  
foraminous endless fabric; and  
20 contacting the moving foraminous endless fabric bearing the deposited nascent  
web with a moving endless pressing blanket engaged with a pressing unit thereby  
forming a nip, the pressing unit being configured to create a peak engagement pressure  
of at least about 2000 kN/m<sup>2</sup> at an overall line load of less than about 240 kN/m.

25 There is also disclosed:  
A method of making an absorbent paper sheet product comprising:  
depositing a nascent web for the absorbent paper sheet product on a moving

5 foraminous endless fabric;  
contacting the moving foraminous endless fabric bearing the deposited nascent web with a moving endless pressing blanket engaged with a pressing unit thereby forming a nip, the pressing unit being configured to create a peak engagement pressure of at least about 2000 kN/m<sup>2</sup> at an overall line load of less than about 240 kN/m;

10 transferring the web to a Yankee drying cylinder; and  
creping the web from the Yankee drying cylinder.

There is finally disclosed:

A method of making an absorbent paper sheet product comprising:  
depositing a nascent web for the absorbent paper sheet product on a moving foraminous endless fabric;  
contacting the moving foraminous endless fabric bearing the deposited nascent web with a shoe press thereby forming a nip between the shoe press and a Yankee drying cylinder, the shoe press being configured to create a peak engagement pressure of at least about 2000 kN/m<sup>2</sup> at an overall line load of less than about 240 kN/m;

15 disengaging the web from the foraminous endless fabric in the nip onto a Yankee drying cylinder;  
drying the web on the Yankee drying cylinder; and  
creping the web from the Yankee drying cylinder.

20 The accompanying drawings are included to provide a further understanding of the invention and are incorporated in and constitute a part of the specification. The drawings illustrate embodiments of the invention and, together with the description,

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serve to explain the principles of the invention.

#### BRIEF DESCRIPTION OF THE DRAWINGS

Figure 1 illustrates a side view of a typical stand alone shoe press.

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Figure 2 illustrates the relationship between peak pressure and line load for a variety of shoe press arrangements found in the literature, as well as for Yankee suction pressure rolls.

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Figure 3 illustrates nip pressure profiles for a suction pressure roll, a typical shoe press, and a shoe press made according to the present invention.

Figure 4 illustrates one conventional wet press processing apparatus.

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Figure 5 illustrates one conventional through-air-drying processing apparatus.

Figure 6 illustrates a typical pressure profile in the nip of a suction pressure roll, backing roll, or transfer cylinder according to the prior art.

Figure 7 illustrates a pressure profile in the nip of a shoe press.

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Figure 8 illustrates a preferred pressure profile in the nip of a shoe press where the negative pressure corresponds to the vacuum level in the felt.

Figure 9 illustrates a shoe press with a large diameter transfer cylinder where the felt rides the web causing rewet after the press nip.

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Figure 10 illustrates a tapered shoe in a shoe press with a large diameter transfer cylinder where the felt is rapidly separated from the web but not from the pressing blanket.

5 Figure 11 illustrates a tapered shoe in a shoe press with a large diameter

transfer cylinder where the felt is simultaneously stripped from the sheet and from the  
pressing blanket on the exit side of the nip.

10 Figure 12 shows a plot of cold Yankee press solids versus line loading for a  
conventional 120 mm shoe, for a 50 mm shoe made according to the present invention,  
and for a suction pressure roll.

15 Figure 13 illustrates a side view of a typical stand alone shoe press with a  
blanket having void space.

20 Figure 14 illustrates a blind drilled blanket or belt.

25 Figure 15 illustrates a grooved blanket or belt.

#### DETAILED DESCRIPTION

In the production of absorbent paper products, paper web drying efficiency and paper web moisture removal directly affect machine speed, and therefore have a significant effect on the productivity that can be attained on a papermachine. The present invention improves paper web moisture removal through the controlled use of a pressing unit in conjunction with a backing roll and/or a transfer cylinder or Yankee drying cylinder. An absorbent paper web as defined herein includes bath tissue, paper towels, paper napkins, wipers, and facial tissue. The basis weight of such products and their base sheets are in the range of about 8 lb/3000ft<sup>2</sup> to about 50 lb/3000ft<sup>2</sup>.

25 According to the present invention, absorbent paper may be produced using any known method or papermaking scheme. The most common papermaking methods are

5 (I) conventional wet pressing (CWP) and (II) through-air-drying (TAD). In a  
conventional wet press process, i.e., apparatus (10), as exemplified in Figure 4, a  
furnish is fed by means not shown through conduits (40, 41) to headbox chambers (20,  
10 20'). A web (W) is formed on a conventional wire former on fabric (12), supported by  
rolls (18, 19), from a liquid slurry of pulp, water and other chemicals. Materials removed  
from the web through fabric (12) in the forming zone are returned to silo (50), from  
15 saveall (22) through conduit (24). The web is then transferred to a moving felt (14),  
supported by roll (11) for pressing and drying. Materials removed from the web during  
pressing or from the Uhle box (29) are collected in saveall (44) and fed to white water  
20 conduit (45). The web is pressed by suction pressure roll (16) against the surface of a  
rotating Yankee dryer cylinder (26), which is heated to cause the paper to substantially  
dry on the cylinder surface. The moisture within the web as it is laid on the Yankee  
surface causes the web to transfer to the surface. Liquid adhesive may be applied to  
the surface of the dryer to provide substantial adherence of the web to the creping  
surface. The web is then creped from the surface with a creping blade (27). The  
25 creped web is then usually passed between calender rollers (not shown) and rolled up  
on reel (28) prior to further converting operations, for example, embossing.

A web may alternatively be subjected to vacuum deformation on an impression  
fabric, alone or in conjunction with other physical deformation processes, and a  
dewatering step which removes water from the web to a solids content of at least about  
25 30% without the need for overall physical compression. This type of process is  
conventionally referred to as a through-air-drying process or TAD process. This

process is generally described in U.S. Patent Nos. 3,301,746 to Sanford et al. and 3,905,863 to Ayers, which are incorporated herein by reference in their entirety.

As an example, one conventional TAD process is illustrated in Figure 5. In this process, fibers are fed from a headbox (10) to a converging set of forming wires (20,30). In this twin wire forming arrangement water is removed from the web by centrifugal forces and by vacuum means. The wet nascent web is cleanly transferred to forming wire (30) via Uhle box (40). The web can be optionally processed to remove water by vacuum box (50) and steam shroud (60). The web is carried along forming fabric (30) until it is transferred to a TAD fabric (70) at junction (80) by means of a vacuum pickup shoe (90). The web is further dewatered at dewatering box (100) to increase web solids. Besides removing water from the web, vacuum pickup shoe (90) and dewatering box (100) inundate the web into TAD fabric (70) causing bulk and absorbency improvements.

Further enhancements in bulk and absorbency can be obtained by operating the speed of the forming section (i.e., the speeds of forming fabrics 20 and 30) faster than the speed of TAD fabric (70). This is referred to as fabric/fabric creping. In this manner the web is inundated and wet shaped into the fabric creating bulk and absorbency. Thickness created by wet shaping is more effective in generating absorbency (i.e. less structural collapse) than thickness created in the dry state, e.g., by conventional embossing. The web is then carried on TAD fabric (70) to drying unit (110) where heated air is passed through both the web and the fabric to increase the solids content of the web. Generally, the web is 30 to 95% dry after exiting drying unit (110). In one

5 process, the web may be removed directly from TAD fabric (70) in an uncreped state.  
In the embodiment shown in Figure 5, the web is transferred from TAD fabric (70) to  
Yankee dryer cylinder (130) and is creped from dryer cylinder (130) via creping blade  
10 (150). The creped web is then usually passed between calender rollers (160) and rolled  
up on reel (170) prior to further converting operations, for example, embossing to make  
roll products.

According to the present invention, an absorbent paper web can be made by dispersing fibers into aqueous slurry and depositing the aqueous slurry onto the forming wire of a paper making machine. Any art recognized forming scheme might be used. For example, an extensive but non-exhaustive list includes a crescent former, a C-wrap twin wire former, an S-wrap twin wire former, a suction breast roll former, a fourdrinier former, or any art recognized forming configuration. The particular forming apparatus is not critical to the success of the present invention. The forming fabric can be any art recognized foraminous member including single layer fabrics, double layer fabrics, triple layer fabrics, photopolymer fabrics, and the like. Non-exhaustive background art in the forming fabric area include U.S. Patent Nos. 4,157,276; 4,605,585; 4,161,195; 15 3,545,705; 3,549,742; 3,858,623; 4,041,989; 4,071,050; 4,112,982; 4,149,571; 20 4,182,381; 4,184,519; 4,314,589; 4,359,069; 4,376,455; 4,379,735; 4,453,573; 4,564,052; 4,592,395; 4,611,639; 4,640,741; 4,709,732; 4,759,391; 4,759,976; 25 4,942,077; 4,967,085; 4,998,568; 5,016,678; 5,054,525; 5,066,532; 5,098,519; 5,103,874; 5,114,777; 5,167,261; 5,199,467; 5,211,815; 5,219,004; 5,245,025; 5,277,761; 5,328,565; and 5,379,808 all of which are incorporated herein by reference

5 in their entirety. The particular forming fabric is not critical to the success of the present invention. One forming fabric found particularly useful with the present invention is Appleton Mills Forming Fabric 2184 made by Appleton Mills Forming Fabric Corporation, Florence, MS.

10 Papermaking fibers used to form the absorbent products of the present invention include cellulosic fibers commonly referred to as wood pulp fibers, liberated in the pulping process from softwood (gymnosperms or coniferous trees) and hardwoods (angiosperms or deciduous trees). Cellulosic fibers from diverse material origins may be used to form the web of the present invention. These fibers include non-woody fibers liberated from sugar cane, bagasse, sabai grass, rice straw, banana leaves, 15 paper mulberry (i.e., bast fiber), abaca leaves, pineapple leaves, esparto grass leaves, and fibers from the genus *Hesperaloe* in the family Agavaceae. Also recycled fibers which may contain any of the above fiber sources in different percentages, can be used in the present invention. Suitable fibers are disclosed in U.S. Patent Nos., 5,320,710 and 3,620,911, both of which are incorporated herein by reference.

20 Papermaking fibers can be liberated from their source material by any one of the number of chemical pulping processes familiar to one experienced in the art including sulfate, sulfite, polysulfide, soda pulping, etc. The pulp can be bleached if desired by chemical means including the use of chlorine, chlorine dioxide, oxygen, etc. Furthermore, papermaking fibers can be liberated from source material by any one of a 25 number of mechanical/chemical pulping processes familiar to anyone experienced in the art including mechanical pulping, thermomechanical pulping, and chemi-

5 thermomechanical pulping. These mechanical pulps can be bleached, if necessary, by  
a number of familiar bleaching schemes including alkaline peroxide and ozone  
bleaching.

10 The suspension of fibers or furnish may contain chemical additives to alter the  
physical properties of the paper produced. These chemistries are well understood by  
the skilled artisan and may be used in any known combination.

15 The pulp can be mixed with strength adjusting agents such as wet strength  
agents, dry strength agents and debonders/softeners. Suitable wet strength agents will  
be readily apparent to the skilled artisan. A comprehensive but non-exhaustive list of  
useful wet strength aids include urea-formaldehyde resins, melamine formaldehyde  
resins, glyoxylated polyacrylamide resins, polyamide-epichlorhydrin resins and the like.  
Thermosetting polyacrylamides are produced by reacting acrylamide with diallyl  
dimethyl ammonium chloride (DADMAC) to produce a cationic polyacrylamide  
copolymer which is ultimately reacted with glyoxal to produce a cationic cross-linking  
wet strength resin, glyoxylated polyacrylamide. These materials are generally  
described in U.S. Patent Nos. 3,556,932 to Coscia et al. and 3,556,933 to Williams et  
al., both of which are incorporated herein by reference in their entirety. Resins of this  
type are commercially available under the tradename of PAREZ 631NC by Cytec  
Industries. Different mole ratios of acrylamide/DADMAC/glyoxal can be used to  
produce cross-linking resins, which are useful as wet strength agents. Furthermore,  
other dialdehydes can be substituted for glyoxal to produce thermosetting wet strength  
characteristics. Of particular utility are the polyamide-epichlorhydrin resins, an example

5 of which is sold under the tradenames Kymene 557LX and Kymene 557H by Hercules  
Incorporated of Wilmington, Delaware and CASCAMID® from Borden Chemical Inc.  
These resins and the process for making the resins are described in U.S. Patent No.  
10 3,700,623 and U.S. Patent No. 3,772,076 each of which is incorporated herein by  
reference in its entirety. An extensive description of polymeric-epihalohydrin resins is  
given in Chapter 2: Alkaline -Curing Polymeric Amine-Epichlorohydrin by Espy in *Wet -*  
15 *Strength Resins and Their Application* (L. Chan, Editor, 1994), herein incorporated by  
reference in its entirety. A reasonably comprehensive list of wet strength resins is  
described by Westfelt in Cellulose Chemistry and Technology, Volume 13, p. 813,  
1979, which is incorporated herein by reference. The pulp, when making towel grades  
15 *Strength Resins and Their Application* (L. Chan, Editor, 1994), herein incorporated by  
reference in its entirety. A reasonably comprehensive list of wet strength resins is  
described by Westfelt in Cellulose Chemistry and Technology, Volume 13, p. 813,  
1979, which is incorporated herein by reference. The pulp, when making towel grades  
15 according to the present invention, preferably contains up to about 30 lbs/ton, more  
preferably from 10 to 20 lbs/ton of wet strength aids. Wet strength resins are not  
normally added to tissue grades.

20 Suitable dry strength agents will be readily apparent to one skilled in the art. A  
comprehensive but non-exhaustive list of useful dry strength aids includes starch, guar  
gum, polyacrylamides, carboxymethyl cellulose and the like. Of particular utility is  
carboxymethyl cellulose, an example of which is sold under the tradename Hercules  
25 CMC by Hercules Incorporated of Wilmington, Delaware. The pulp preferably contains  
from 0 to 10 lbs/ton, more preferably from 1 to 5 lbs/ton of dry strength aid.

25 Suitable debonders will be readily apparent to the skilled artisan. Debonders or  
softeners may also be incorporated into the pulp or sprayed upon the web after its  
formation. The pulp preferably contains from 0 to 10 lbs/ton, more preferably from 1 to

5

5 lbs/ton of debonder/softener.

10

The present invention may be used with a particular class of softener materials - amido amine salts derived from partially acid neutralized amines. Such materials are disclosed in U.S. Patent No. 4,720,383. Evans, Chemistry and Industry, 5 July 1969, Pp. 893-903; Egan, J. Am. Oil Chemist's Soc., Vol. 55 (1978), Pp. 118-121; and Trivedi et al., J. Am. Oil Chemist's Soc., June 1981, Pp. 754-756, incorporated by reference in their entirety, indicate that softeners are often available commercially only as complex mixtures rather than as single compounds. While the following discussion will focus on the predominant species, it should be understood that commercially available mixtures would generally be used in practice.

20

Quasoft 202-JR is a suitable softener material, which may be derived by alkylating a condensation product of oleic acid and diethylenetriamine. Synthesis conditions using a deficiency of alkylation agent (e.g., diethyl sulfate) and only one alkylation step, followed by pH adjustment to protonate the non-ethylated species, result in a mixture consisting of cationic ethylated and cationic non-ethylated species. A minor proportion (e.g., about 10%) of the resulting amido amine cyclize to imidazoline compounds. Since only the imidazoline portions of these material are quaternary ammonium compounds, the compositions as a whole are pH-sensitive. Therefore, in the practice of the present invention with this class of chemicals, the pH in the headbox should be approximately 6 to 8, more preferably 6 to 7 and most preferably 6.5 to 7.

25

Quaternary ammonium compounds, such as dialkyl dimethyl quaternary ammonium salts are also suitable particularly when the alkyl groups contain from about

5 14 to 20 carbon atoms. These compounds have the advantage of being relatively  
insensitive to pH.

10 Biodegradable softeners can be utilized. Representative biodegradable cationic  
softeners/debonders are disclosed in U.S. Patent Nos. 5,312,522; 5,415,737;  
15 5,262,007; 5,264,082; and 5,223,096, all of which are incorporated herein by reference  
in their entirety. These compounds are biodegradable diesters of quaternary ammonia  
compounds, quaternized amine-esters, and biodegradable vegetable oil based esters  
20 functional with quaternary ammonium chloride and diester dierucyldimethyl ammonium  
chloride and are representative biodegradable softeners.

25 The fibrous web is then either deposited on an impression drying fabric, in the  
case of the TAD process or on a dewatering felt for the CWP process. Any art  
recognized fabrics or felts could be used with the present invention. For example, a  
non-exhaustive list of impression fabrics would include plain weave fabrics described in  
U.S. Patent No. 3,301,746; semitwill fabrics described in U.S. Patent Nos. 3,974,025  
and 3,905,863; bilaterally-staggered-wicker-basket-cavity type fabrics described in U.S.  
Patent Nos. 4,239,065 and 4,191,609; sculptured/load bearing layer type fabrics  
described in U.S. Patent No. 5,429,686; photopolymer fabrics described in U.S. Patent  
Nos. 4,529,480, 4,637,859, 4,514,345, 4,528,339, 5,364,504, 5,334,289, 5,275,799,  
and 5,260,171; and fabrics containing diagonal pockets described in U.S. Patent No.  
5,456,293. The aforementioned patents are incorporated herein by reference, in their  
entirety. Any art-recognized-felt can be used with the present invention. For example,  
felts can have double-layer base weaves, triple-layer base weaves, or laminated base

5 weaves. Preferred felts according to the present invention are those having the  
laminated base weave design. A wet-press-felt found particularly useful with the  
present invention is AMFlex 3 made by Appleton Mills Corporation. Non-exhaustive  
background art in the press felt area includes U.S. Patent Nos. 5,657,797; 5,368,696;  
10 4,973,512; 5,023,132; 5,225,269; 5,182,164; 5,372,876; and 5,618,612 all-of-which are  
incorporated herein by reference in their entirety. After the web made by the  
conventional wet press process has reached a solids content of about 15 %, more  
preferably about 20 %, the web/foraminous fabric sandwich is contacted with a pressing  
blanket engaged with a pressing unit, one embodiment in the art referred to as a shoe  
press. In a similar web made by through air drying, the web/foraminous fabric sandwich  
15 is preferably contacted with the pressing blanket engaged with a pressing unit after the  
web has reached a solids content of at least about 20%, more preferably at least about  
25%.

20 The pressing unit including a pressing blanket according to the present invention  
can have any art-recognized configuration. The nip can be created between the  
pressing unit and a backing roll, in the case of a stand-alone pressing unit, or can be  
created between the pressing unit and a transfer cylinder. As used in the present  
invention, backing roll refers to a roll that contacts the web but does not remove the  
fibrous web from the carrier fabric or felt. Backing rolls for use according to the present  
25 invention may be heated or cold. The backing roll can be made of hard rubber or metal.  
When the rolls are heated with an induction heater the roll is preferably constructed or  
coated with high diffusivity material, such as copper, to aid in increasing heat transfer.

5 As used in the present invention, transfer cylinder refers to a roll that picks up the fibrous web thereby transferring the fibrous web from the porous carrier fabric upon which it had been carried. Typical transfer cylinders according to the present invention can include a steel roll, a metal coated roll, a granite roll, a Yankee drying cylinder, and a gas fired drying cylinder. Transfer cylinders for use according to the present method  
10 may be heated or cold. When the transfer cylinder is heated with an induction heater the cylinder is preferably constructed or coated with high diffusivity material, such as copper, to aid in increasing heat transfer. One or more transfer cylinders may be used in the process according to the present invention.

15 Heat is preferably applied to the transfer cylinder and/or backing roll. Heat can be applied by any art-known scheme including induction heating, oil heating and steam heating. Commercial available induction heaters can generate very high energy-transfer rates. An induction heater induces electrical current to the conducting roll surface. Since the induced current can be quite large, this factor produces a substantial amount of resistive heating in the conducting roll. Backing roll or transfer cylinder temperature can be anywhere from ambient to 700 ° F but are more preferably from 180 ° F to 500 ° F. Preferred heating schemes according to the present invention are induction heating and steam-heating.

20

25 Increased temperature in the backing roll or transfer cylinder decreases the viscosity of the water and makes the sheet more deformable hence improving water removal. Also, increased temperature and operating pressure bring the sheet into intimate contact with the transfer cylinder or backing roll, which improves heat transfer

5 to the web. Furthermore, high steam pressure in the web within the nip can aid in rapidly displacing water from the sheet to the felt.

10 The pressing unit including a pressing blanket according to the present invention is preferably a shoe press. A shoe press includes a shoe element(s), which is pressed against the backing roll or transfer cylinder. The shoe element is loaded hydrodynamically against the backing roll or transfer cylinder causing a nip to be formed. A pressing belt or blanket traverses the shoe press nip with the fibrous web in contact with the foraminous fabric.

15 Pressing blankets can be smooth, or to enhance water removal at the press they can be grooved or blind drilled. Conventional pressing blanket designs contain a fabric coated with polyurethane where the fabric is used as reinforcement. Other pressing blanket designs use yarns embedded in the polyurethane to provide reinforcement. One preferred pressing blanket according to the present invention is a yarn reinforced blanket design under the tradename QualiFlex B, which is supplied by Voith Sulzer Corporation.

20 The shoe element length can be less than about 7 inches but is more preferably less than about 3 inches for the present invention. According to the present invention the shoe element will also be referred to as a hydraulic engagement member. Shoe designs can be hydrodynamic, hydrodynamic pocket, or hydrostatic. In the hydrodynamic shoe design, the oil lubricant forms a wedge at the ingoing side of the nip ultimately causing the formation of a thin oil film that protects the blanket and the shoe. The hydrodynamic pocket design incorporates a machined full width pocket in the shoe

5 used for emptying the oil in the pressurized zone of the shoe. The final design is the hydrostatic design where oil is fed into the center region of the shoe. The preferred shoe design according to the present invention is hydrodynamic.

Shoe presses for use according to the present invention can be open or closed. Early shoe press designs were the open belt configurations where an impermeable 10 pressing blanket encircled a series of rollers similar to that of a fabric or felt run. These open designs suffered from papermachine system contamination by oil. The oil loss was at one time, up to 20 liters per day on some systems. The open shoe design is also inferior to a closed design since it cannot be operated in the inverted mode. The closed shoe design alleviates the oil contamination issue and is therefore preferred for 15 use in the present invention.

According to one embodiment of the present invention, the peak pressure in the shoe press is preferably greater than about 2000 kN/m<sup>2</sup>, with a line load of preferably less than about 240 kN/m. In another embodiment of the present invention, for 20 conventionally made wide-Yankee-dryers the peak pressure is preferably greater than about 2000 kN/m<sup>2</sup>, while the line load is preferably less than about 175 kN/m and more preferably less than about 100 kN/m. For the purposes of the present invention, kN/m is an abbreviation for kilonewtons per meter and kN/m<sup>2</sup> is an abbreviation for kilonewtons per square meter.

25 The sheet can be creped from the transfer cylinder by any art-recognized methods using any art recognized creping aid.

The maximum line load a current standard Yankee can sustain is on the order of

5 100kN/m. When a Yankee is used in conjunction with a suction pressure roll, the  
Yankee needs to be precisely crowned at the prevailing load to obtain a uniform nip.  
This procedure is necessary due to the inflexibility of the suction pressure roll  
arrangement and also due to loading at only the ends of the suction pressure roll. For  
the case of a shoe press, loading occurs at multiple points across the cross machine  
10 direction; individual shoe elements can be installed across the machine to give more  
precise cross machine direction pressing flexibility; and the shoe press is flexible and  
capable of conforming to the Yankee dryer surface. As a result, the precision to which  
the Yankee is ground for crowning will be less.

15 Figure 6 shows a schematic sketch of a typical pressure distribution curve for a  
suction pressure roll described by symmetrical mathematical functions like the sine and  
haversine curves. Since the nip pressure is relieved when the nip diverges, rewet is  
exacerbated for the suction pressure roll. Figure 7 shows a schematic sketch of a  
pressure distribution curve for a shoe press with a steep drop off where the felt is  
stripped from the sheet and later from the pressing blanket. Such a steep drop-off in  
20 pressure reduces the amount of rewet. Figure 8 shows a schematic sketch of a  
pressure distribution curve for a shoe press with a steeper drop off and where suction  
occurs in the felt at the point of simultaneous separation of the felt, sheet, and blanket  
when the nip pressure reaches about zero. The negative pressure in the felt, when the  
blanket and felt are stripped apart, is caused by capillary forces and should aid in  
holding water in the felt and should help further dewater the web.

25 Previous shoe, belt or blanket, and felt designs in wide nip presses do not permit

5 optimum separation of these members. For instance, present designs allow for quick  
separation of the felt and blanket since the felt cannot "wrap" the unsupported blanket.  
But the drawback is that the felt stays in contact with the sheet allowing capillary flow  
back into the sheet, i.e., rewet (see Figure 9). Figure 9 is a schematic sketch of a shoe  
press nip showing sheet, felt, and blanket. Point A in Figure 9 is the point of zero  
10 pressure on the pressure distribution curve at the exit side of the nip.

Rewet is determined in the literature by plotting moisture ratio versus the  
reciprocal of the basis weight using the following equation:

$$K_p = K_o + R/W$$

15 where  $K_p$  is the moisture ratio of the paper after the wet press in grams of water per  
gram of fiber;  $K_o$  is the moisture ratio of paper for  $1/W = 0$ ;  $W$  is the basis weight in  $g/m^2$ ;  
and  $R$  is the magnitude of the rewet of paper in  $g/m^2$  and corresponds to the slope of  
the straight line used to fit moisture ratio versus reciprocal basis weight data. The  
aforementioned equation was first established by John Sweet. Data plotted according  
to the above equation is frequently referred to in the literature as a Sweet plot. The  
20 original work can be found in Sweet, J.S., Pulp and Paper Mag. Can., 62, No. 7: T267  
(1961) and a review article can be found in Heller, H., MacGregor, M., and Bliesner, W.,  
Paper Technology and Industry, p.154, June, 1975. Rewet is much more significant for  
lightweight tissue grades than heavy weight linerboard grades. Rewet has been  
estimated to be from 5 to 50  $g/m^2$  of water, depending on the felt, furnish, etc. Rewet  
25 for a conventional shoe press can be determined from the above equation. The  
amount of rewet for the optimum shoe press is preferably less than about 50 % of the

amount determined from Sweet's theory using a conventional shoe press system.

Rewet is preferably from 0 to 10 g/m<sup>2</sup> of water, more preferably from 0 to 5 g/m<sup>2</sup> of water.

According to another embodiment of the present invention, a pressing felt wraps the blanket and, therefore, pulls away quickly from the sheet reducing the time for possible rewetting. This design, as depicted in Figure 10, can be achieved by altering the take-away angle of the felt from the nip and tapering the exit side of the shoe. To aid in blanket deflection from the felt at the exit side of the shoe, the blanket diameter can be reduced; the blanket can be eccentrically arranged with respects to the press plane; or a roll (not shown in Figure 10) positioned against the blanket can deflect the belt further.

Figure 11 shows another embodiment according to the present invention. In Figure 11, a schematic sketch of a shoe press showing a sheet, felt, and blanket is displayed. This shoe press utilizes a very steep pressure drop at and following the exit of a nip curve of the press while simultaneously, separating the felt from the blanket and from the sheet. In this manner, the negative pressure generated by surface tension forces as the felt and blanket separate are effective in reducing the flow of water back into the sheet as the felt and sheet are separated. The drawing shows a sharp drop off of the blanket near the shoe which in turn permits a quick separation of the felt from both the blanket and the sheet. The outgoing felt would be pulled at an angle that equally bisected the Yankee and blanket surfaces. Then by adjusting the tension on the felt, the exact point of separation can be controlled to affect the minimum

5 in rewet. A felt drive roll located immediately following the shoe press can control the tension level on the felt. The objective of this embodiment according to the present invention is to affect the transfer of the sheet from the felt at the same time that the negative pulse caused by the separation of the felt and blanket occurs. This design not only minimizes the time the felt is in contact with the sheet; the added vacuum pulse will 10 significantly reduce the amount of water that can flow, even over the short time. Point A in Figure 11 is the point of zero pressure on the pressure distribution curve at the exit side of the nip. The nip pressure curve for the sheet/felt in Figure 11 would most likely approach that shown in Figure 8.

15 The web is preferably either adhered to the Yankee dryer by nip transfer with a pressing unit including a pressing blanket or is after pressing adhered to the Yankee dryer. The web is dried by steam and hot air impingement hoods. Any suitable art recognized adhesive might be used on the Yankee dryer. Preferred adhesives include polyvinyl alcohol with suitable plasticizers, glyoxylated polyacrylamide with or without polyvinyl alcohol, and polyamide epichlorohydrin resins such as Quacoat A-252 20 (QA252), Betzcreplus 97 (Betz+97) and Calgon 675 B. Suitable adhesives are widely described in the patent literature. A comprehensive but non-exhaustive list includes U.S. Patent Nos. 5,246,544; 4,304,625; 4,064,213; 3,926,716; 4,501,640; 4,528,316; 4,788,243; 4,883,564; 4,684,439; 5,326,434; 4,886,579; 5,374,334; 4,440,898; 25 5,382,323; 4,094,718; 5,025,046; and 5,281,307. Typical release agents can be used in accordance with the present invention.

The final product may be calendered or uncalendered and is usually reeled to

5 await further converting processes. The products according to the present invention  
may be subjected to any art recognized converting operations, including embossing,  
printing, etc.

The following example is illustrative of the invention embodied herein.

10 EXAMPLE 1

A nascent web was formed on a Crescent-forming machine using a blend of  
50/50 long fiber/short fiber refined to 23° SR freeness. Chemicals like wet strength  
agents or dry strength agents were not added to the stock. The basis weight of the  
sheet on the Yankee dryer was 8.5 lbs/3000 ft<sup>2</sup>. Two pressing arrangements were used  
15 on the paper machine. In the first pressing arrangement, the sheet was pressed onto a  
Yankee dryer with a suction pressure roll. The vacuum in the suction roll was nominally  
0.22 bar. In the second pressing arrangement, the suction pressure roll was replaced  
by a Yankee shoe press. The sheet was conditioned before the shoe press with a  
suction turning roll having the same size and open area as the suction pressure roll.  
The suction turning roll vacuum was nominally equivalent to the level used during the  
20 suction pressure roll experiments. After sheet conditioning, the web was pressed onto  
the Yankee with a shoe press. In order to obtain precise sheet solids data after the  
shoe press or the suction pressure roll, the Yankee dryer was run cold. Blotters were  
used to collect flatsheets for physical property determination. Two types of shoes were  
25 run: a typical 120 mm shoe and a 50 mm shoe. Figure 3 shows the pressure  
distribution of the shoes and the suction pressure roll. Figure 12 depicts a plot of sheet

5       solids versus line loading. The typical 120 mm shoe shows no solids benefit versus the suction pressure roll at present operating line load limits of current Yankee dryers (i.e., approximately, 87.5 kN/m), while the 50 mm pressure optimized shoe press shows an advantage of several percentage points of solids. Furthermore, the strength and specific volume properties of a web made with the 50 mm pressure optimized shoe  
10      press were equivalent to the strength and specific volume properties of a web made by the suction pressure roll.

15      Figures 13-15 illustrate a method for maximizing water removal in a press nip in accordance with another embodiment of the present invention. The present embodiment involves a conventional wet pressing (CWP) process. For consistency, like numbers have been used to indicate the corresponding portions of the apparatus depicted in Figures 13-15 with those of Figures 1-12. The description of the apparatus of Figures 1-12 thus applies equally to this embodiment, unless stated otherwise.

20      Referring to Figure 13, the present embodiment uses a shoe press, preferably a controlled crown roll with a flexible shell and a concave shoe hydrodynamically loaded against one another. The present embodiment further includes a belt or blanket (100) having a void volume that enhances sheet solids after the shoe press to further improve water removal in the press nip. Appropriate void volume can be achieved by a number of blanket configurations, including, but not limited to, those made by grooving, blind drilling and the like. The total void volume of the belt or blanket for use according to the present invention is preferably about 50 to about 3000 cm<sup>3</sup>/m<sup>2</sup>, more preferably about 25      100 to about 1000 cm<sup>3</sup>/m<sup>2</sup>, most preferably from about 200 to about 500 cm<sup>3</sup>/m<sup>3</sup>.

Blankets for use according to the present invention can include any art recognized blanket having, or which can be modified to have, the required void volume.

For example, blankets disclosed by E.J. Justus and D. Cronin in Tappi, August 1964, Vol. 47, No. 8, p. 493, which is incorporated herein by reference, include grooved belts that improve water removal in a press nip where the groove width is about 0.01 to about 0.03 in., the land width is about 2 to about 20 times the groove width and the groove depth is about 2 to about 10 times the groove width.

For another example, blankets disclosed by Bo-Christer Aberg in Das Papier No. 6, 1996, which is incorporated herein by reference, include grooved belts that work at higher line loads and machine speeds than smooth belts. The belts have groove widths of about 0.5 to about 1 mm and a void volume of about 100 cc/m<sup>2</sup> to about 500 cc/m<sup>2</sup>.

For yet another example, blankets disclosed by P. Slater and K. Fitzpatrick in the 84<sup>th</sup> Annual Meeting of the Technical Section, CPPA, January 1998, which is incorporated herein by reference, include grooved belts that provide a press dryness about 1% to about 3% greater than the press dryness obtained with a similar smooth belt. The belts have groove widths of about 0.58 to about 0.79 mm and a void volume of about 200 cc/m<sup>2</sup> to about 365 cc/m<sup>2</sup>.

For still another example, blankets disclosed by D. Madden et al. in the Tappi 1998 Engineering Conference, which is incorporated herein by reference, include grooved belts that provide a press dryness about 1% greater than the dryness obtained with a blind drilled belt. The grooved belt has an open area of about a 20.3% and a

5 void volume of about 260 cc/m<sup>2</sup>, and the blind drilled belt has an open area of about  
21% and a void volume of about 380 cc/m<sup>2</sup> void volume.

10 Referring to Figure 14, blind drilling involves drilling holes into a smooth blanket, as will be understood by one of skill in the art. Nip compression between a blind drilled blanket and the felt causes a hydraulic pressure gradient between the holes in the  
blanket and the felt which improves water flow and removal.

15 The blind drilled blanket preferably has a plurality of holes sequentially arranged in the machine direction and a plurality of rows sequentially arranged in the cross-machine direction to cause a hydraulic pressure gradient. The blind drilled blanket can take a variety of configurations. For example, the hole depth, hole diameter, hole spacing, hole angle, hole geometry, row spacing and/or row pattern can be varied.

20 In particular, the hole depth can range from about 0.2 to about 10 mm, more preferably about 0.5 to about 5 mm, most preferably from about 0.5 to about 3 mm. Also, the hole depth can extend partially or completely through the blanket.

25 The hole diameter can range from about 0.2 to about 10 mm, more preferably about 0.5 to about 5 mm, most preferably from about 1 to about 3 mm.

The hole spacing can range from about 1 to about 20 mm between holes arranged within the same row, more preferably about 1 to about 10 mm, most preferably from about 1 to about 5 mm.

25 The hole angle (i.e., the angle measured from the surface of the belt material counterclockwise to the side of the hole) can range from about 45 to about 135 degrees along any wall in either the machine or cross-machine, more preferably about 70 to

5 preferably about 0.2 to about 5 mm, most preferably from about 0.4 to about 3mm.

10 The groove width can range from about 0.1 to about 6 mm, more preferably about 0.2 to about 4 mm, most preferably from about 0.4 to about 3 mm.

15 The groove bevel (i.e., the angle measured from the surface of the belt material counterclockwise to the side of the groove minus 90°) can range from about 0 to about 45°, more preferably about 0 to about 30°, most preferably from about 0 to about 20°.

20 The groove angle can range from about 45 to about 135 degrees (with 90 degrees being orthogonal to the cross-machine direction), more preferably about 65 to about 115°, most preferably from about 80 to about 100°.

25 The land width can range from about 0.2 to about 25 mm, more preferably about 0.4 to about 10 mm, most preferably from about 0.6 to about 4 mm.

30 The open area can range up to 80% of the total blanket area, more preferably about 15 to about 50%, most preferably from about 20 to about 40%.

35 The groove pattern can be such that the grooves in each row are aligned in the cross-machine direction, offset in the cross-machine direction, aligned in the machine direction, offset in the machine direction and the like. Also, for blankets for use in the present invention, grooves need not have the same configuration, rather, all the grooves can have a different configuration, or one or more individual or set of grooves can have the same configuration as one or more other individual or set of grooves.

40 Further, there is no requirement that the groove pattern form any type of geometric or other pattern, for example, the groove placement can also be random.

45 Blankets having the disclosed void volume will be readily apparent to the skilled

5 artisan. Such blankets can include any physical arrangement as long as the void space requirements are satisfied. Blankets for use in the present invention may be manufactured by any art recognized process, including but not limited to, casting molding, laser engraving, etc.

10 EXAMPLE 2

15 A punch press was used to perform dewatering experiments with different belt structures. An AMFlex 3S felt manufactured by Appleton Mills Corporation was used to dewater the paper web. The web basis weight was 8.9 lbs/rm. The felt dryness was controlled to 69.3% dryness by using blotters and a couch roll to remove excess water. Web moisture was controlled to 19.3% dryness by rewetting moist webs using a water spray. The webs were made from a 50/50 blend of northern softwood kraft and eucalyptus refined in a PFI mill to 510 ml CSF.

20 A smooth belt, a blind drilled belt and a grooved belt were used in the punch press experiment. The blind drilled belt had a bore area of  $3.82 \text{ mm}^2$ , a bore depth of 1.76 mm, an open area of 22.73% and a void volume of  $402.9 \text{ cc/m}^2$ . The grooved belt had a groove width of 0.66 mm, a groove depth of 1.41 mm, a pitch of 0.33 grooves/mm, an open area of 21.78%, and a void volume of  $270.6 \text{ cc/m}^2$ .

25 The punch press was operated such that the average nip pressure was fixed at 400 psi and the average nip dwell time was fixed at 1.8 ms. The experimental post press dryness results for the experiment were:

smooth belt      31.0 +/- 0.30%

5

blind drilled belt 39.2 +/- 0.28%

grooved belt 40.3 +/- 0.42%

with the +/- percentage being the 95% confidence limit for the test.

10

These results indicate that pressing with either a blind drilled or grooved belt leads to enhanced sheet solids when compared to a smooth belt. These results also indicate that pressing with a grooved belt leads to enhanced sheet solids over a blind drilled belt.

Other embodiments of the invention will be apparent to those skilled in the art from consideration of the specification and practice of the invention disclosed herein. It is intended that the specification and examples be considered as exemplary only, with the true scope and spirit of the invention being indicated by the following claims.

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